C.P. No. 362
(18,531)
A.R.C Technical Report

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MINISTRY OF SUPPLY

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Assessment of the Possibility of Using Suction to Inhibit Cavitation on Cylindrical Sections

By

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LONDON : HER MAJESTY'S STATIONERY OFFICE

1957

THREE SHILLINGS NET

ADMIRALTY RESEARCH LABORATORY,

C.P. No. 362

A.R.L/R1/G/HY/18/3

ASSESSMENT OF THE POSSIBILITY OF USING SUCTION TO INHIBIT CAVITATION ON CYLINDRICAL SECTIONS

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ABSTRACT

This report assesses the possibility of using suction to reduce the suction peak in the pressure distribution on a body moving in a fluid, with a view to delaying the onset of cavitation. Two cases are considered:

(1) flow past elliptic cylinders with suction applied over the entire forward half, and

(2) flow past circular cylinders with suction applied over limited areas.

Results are given of calculations made to determine the effect of varying amounts of suction as well as, in the case of (2), the added effect of changing the location and extent of the suction area. It is shown that while the onset of cavitation can be considerably delayed, the amount of suction required to effect such an improvement proves to be excessive. For this reason, it is unlikely that the method can find application; at least, not on non-lifting two-dimensional forms.

ASSESSMENT OF THE POSSIBILITY OF USING SUCTION TO INHIBIT CAVITATION ON CYLINDRICAL SECTIONS

INTRODUCTION

1.1 The inception of cavitation on a body moving in a fluid can be delayed by reducing the suction peak in the pressure distribution. In this report, the possible use of distributed suction is investigated as a means to this end.

1.2 The investigation deals with flow past elliptic cylinders with suction applied over the entire forward half of the cylinder. In addition, and for circular cylinders only, a computing programme was undertaken to determine the effect of suction when applied over limited areas of the surface: in particular, the effect on the suction peak of changing the location and extent of the suction area was considered. Results are given, for both cases, to show the extent by which the free stream speed can be increased before the onset of cavitation for various rates of suction.

1.3 In the assessment it has been assumed that the flow round the cylinder is potential flow. This assumption is inevitable as a first approach to the problem. In many practical cases, however, it would be necessary to ensure that it would be approximately fulfilled to avoid cavitation in the wake: this could be achieved by a relatively small amount of suction over the rear half of the cylinder.

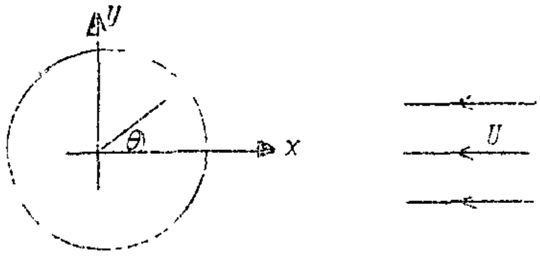
THEORETICAL CONSIDERATIONS

2.1 In this section, theoretical expressions will be derived for two-dimensional potential flow past an elliptic cylinder with suction distributed over the entire forward half.

2.2 Distributed suction will be represented by a distribution of sinks; if a continuous distribution of sinks is taken, then the resulting velocity distribution will also be continuous. A sink distribution of strength proportional to $\cos \eta$ for $0 \leq \eta \leq \pi/2$ and equal to zero for $\pi/2 < |\eta| < \pi$ satisfies this condition, where η is the eccentric angle of the ellipse with $\eta = 0$ giving the forward stagnation point.

2.3 The theoretical problem then is to consider two-dimensional potential flow past an elliptic cylinder with a sink distribution over the forward half of strength proportional to $\cos \eta$. The analysis will be simplified by considering, in the first place, flow past a circular cylinder and then using the methods of conformal transformation to obtain the corresponding flow past an elliptic cylinder.

2.4 Consider a circular cylinder given by $|Z| = a$ in a uniform stream whose velocity at infinity is U in the negative x-direction. It is a well-known result



that the speed of q at any point $Z = ae^{i\theta}$ on the surface of the cylinder is given by

$$q = 2U \sin\theta \qquad \text{...... (1)}$$

2.5 Consider next the problem of flow past a circular cylinder with two sinks of strength m located at points $Z = ae^{i\alpha}$ and $Z = ae^{-i\alpha}$ on the surface. The complex potential of such a flow is

$$W = U\left[Z + \frac{a^2}{Z}\right] + 2m \log (Z - ae^{i\alpha}) + 2m \log (Z - ae^{-i\alpha}) - 2m \log Z$$

and the tangential speed q_t at any point $Z = ae^{i\theta}$ can be shown to be

$$q_t = 2 \sin \theta \left\{U + \frac{m}{a} \cdot \frac{1}{\cos \theta - \cos \alpha}\right\} \qquad \ldots\ldots (2)$$

If the sink strength is $m \cos \alpha$, the tangential speed at $Z = ae^{i\theta}$ is given by

$$q_t = 2 \sin \theta \left\{U + \frac{m}{a} \frac{\cos \alpha}{\cos \theta - \cos \alpha}\right\} \qquad \ldots\ldots (3)$$

2.6 Extending the problem to one of uniform flow past a circular cylinder with a distribution of sinks over the forward half of strength $m \cos \alpha$ per unit arc length, the tangential speed q_t induced at any point P $(Z = ae^{i\theta})$, is obtained by integrating the expression for the speed induced at P by two symmetrically placed elementary sinks each of length $a\, d\alpha$. It follows from equation (3), that the tangential speed is

$$2 \sin \theta \left\{U + m \frac{\cos \alpha \, d\alpha}{\cos \theta - \cos \alpha}\right\}$$

On integrating,

$$q_t = 2 \sin \theta \, (U + m\, I) \qquad \ldots\ldots (4)$$

where

$$I = \int_0^{\pi/2} \frac{\cos \alpha}{\cos \theta - \cos \alpha} \, d\alpha = -\frac{\pi}{2} + \int_0^{\pi/2} \frac{\cos \theta}{\cos \theta - \cos \alpha} \, d\alpha$$

This integral can be evaluated to give

$$I = -\frac{\pi}{2} - \begin{cases} 2 \cot \theta \coth^{-1} \cot \frac{\theta}{2} & \text{for } 0 < \theta < \frac{\pi}{2} \\ 2 \cot \theta \tanh^{-1} \cot \frac{\theta}{2} & \text{for } \frac{\pi}{2} < \theta < \pi \end{cases}$$

In addition there is a normal velocity given by

$$q_n = \begin{cases} m\, \pi \cos \theta & \text{for } 0 < |\theta| < \frac{\pi}{2} \\ 0 & \frac{\pi}{2} \leq |\theta| \leq \pi \end{cases} \qquad \text{(see Ref. 1)}. \qquad \ldots\ldots (5)$$

The resultant speed q at P can now be obtained from equations (4) and (5) and is given by

$$q = \sqrt{q_t^2 + q_n^2} \, . \qquad \ldots\ldots (6)$$

2.7 The solution of the problem of flow past an elliptic cylinder can now be deduced from the solution already obtained for a circle. Consider the conformal transformation

$$Z = \tfrac{1}{2} (z + \sqrt{z^2 - c^2}) \quad \text{with} \quad c^2 = a^2 - b^2 \qquad \ldots\ldots (7)$$

This transformation maps the region outside the ellipse of semi-axes a, b in the z plane into the region outside the circle of radius $\frac{1}{2}(a+b)$ in the Z plane. Furthermore, any point P on the ellipse can be expressed in terms of the eccentric angle η as $z = a\cos\eta + ib\sin\eta$, and corresponds to a point P' on the circle given by $Z = \frac{1}{2}(a+b)\,e^{i\eta}$. Again, if ds and ds' are corresponding elements of length containing P and P' respectively, then

$$\frac{ds}{ds'} = \left|\frac{dz}{dZ}\right| = \left|\frac{-a\sin\eta + ib\cos\eta}{\frac{1}{2}(a+b)\,e^{i\eta}}\right| = \frac{\sqrt{a^2\sin^2\eta + b^2\cos^2\eta}}{\frac{1}{2}(a+b)}$$

Hence, a sink distribution of strength $m\cos\eta$ per unit length on the ellipse corresponds to a sink distribution of strength

$$\frac{m\cos\eta\sqrt{a^2\sin^2\eta + b^2\cos^2\eta}}{\frac{1}{2}(a+b)} \quad \text{per unit length on the circle.}$$

If q, q' be the speeds at P and P' respectively, then

$$q = q'\left|\frac{dZ}{dz}\right| = q'\,\frac{\frac{1}{2}(a+b)}{\sqrt{a^2\sin^2\eta + b^2\cos^2\eta}} \qquad \ldots\ldots (8)$$

2.8 It follows from equations (4), (5) and (6), that the speed q' at P' is given by

$$q' = \sqrt{q'^2_t + q'^2_n}$$

where

$$q'_t = 2\sin\eta\,(U + mJ) \text{ with } J = \int_0^{\pi/2} \frac{\cos\alpha\sqrt{a^2\sin^2\alpha + b^2\cos^2\alpha}}{\frac{1}{2}(a+b)} \cdot \frac{d\alpha}{\cos\eta - \cos\alpha}$$

and

$$q'_n = \begin{cases} \dfrac{m\pi\cos\eta\sqrt{a^2\sin^2\eta + b^2\cos^2\eta}}{\frac{1}{2}(a+b)} & \text{for } -\dfrac{\pi}{2} < \eta < \dfrac{\pi}{2} \\ 0 & \text{for } \dfrac{\pi}{2} \leq \eta \leq \dfrac{3\pi}{2} \end{cases}$$

Hence, since q and q' are related by the expression given in (8), the speed q at any point of the ellipse (given in terms of its eccentric angle η) is

$$q = \sqrt{q_t^2 + q_n^2} \qquad \ldots\ldots (9)$$

where $$q_t = 2\sin\eta\,(U + mJ)\,\frac{\frac{1}{2}(a+b)}{\sqrt{a^2\sin^2\eta + b^2\cos^2\eta}}$$

and $$q_n = \begin{cases} m\pi\cos\eta & \text{for } -\dfrac{\pi}{2} < \eta < \dfrac{\pi}{2} \\ 0 & \text{for } \dfrac{\pi}{2} \leq \eta \leq \dfrac{3\pi}{2} \end{cases}$$

The integral J can be solved in terms of complete elliptic integrals: the solution is

$$\left(\frac{a+b}{2\pi}\right)J = Kk^2\cos^2\eta + k\cos\eta\ln\left(\frac{k'}{1-k}\right) + \cot\eta\sqrt{1-k^2\cos^2\eta}\left[\ln\left|\frac{\sqrt{1-k^2}\cos\eta}{\sin\eta + \sqrt{1-k^2\cos^2\eta}}\right| - KZ\left(\frac{\pi}{2} - \eta, k\right)\right] - E$$

where $K = \int_0^{\pi/2} \frac{d\alpha}{\sqrt{1 - k^2 \sin^2 \alpha}}$ is the complete elliptic integral of the first kind,

$E = \int_0^{\pi/2} \sqrt{1-k^2 \sin^2 \alpha}\, d\alpha$ is the complete elliptic integral of the second kind,

and $Z(\beta,k)$, the Jacobian Zeta function, is defined as

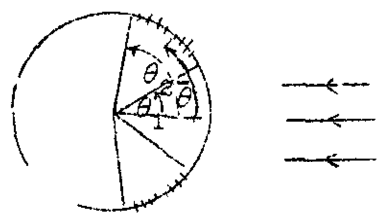
$$Z(\beta,k) = E(\beta,k) - \frac{E}{K} F(\beta,k).$$

2.9 In the absence of suction, it follows from equation (1) using the transformation in (7), that the speed at any point on the elliptic cylinder defined by its eccentric angle η is

$$q = 2U \sin\eta \frac{\frac{1}{2}(a+b)}{(a^2 \sin^2\eta + b^2\cos^2\eta)^{\frac{1}{2}}}. \qquad \ldots\ldots (10)$$

3.1 In this section, equations will be derived for flow past a circular cylinder with suction applied through two areas which are located symmetrically with respect to the fore-and-aft plane of symmetry but which do not in general cover the entire front half of the cylinder.

3.2 Let the extremities of one such area be given by angular co-ordinates θ_1 and θ_2,



then the other suction area is given by co-ordinates $-\theta_1$ and $-\theta_2$. $(\theta_2 - \theta_1)$ will then be a measure of the width of the suction area. If

$$\bar{\theta} = \frac{\theta_1 + \theta_2}{2}$$

$\bar{\theta}$ gives its location.

3.3 Consider flow past a circular cylinder with a distribution of sinks on the surface from $\alpha = \theta_1$ to $\alpha = \theta_2$ and from $\alpha = -\theta_1$ to $\alpha = -\theta_2$ of strength

$$m \cos\left[\left(\frac{|\alpha| - \bar{\theta}}{\theta_2 - \theta_1}\right)\pi\right]$$

per unit arc length. This suction distribution falls to zero at its edges and thus the possibility of an infinite suction peak at these points is avoided.

3.4 From 2.6(4), it follows that

$$\frac{q_t}{U} = 2\sin\theta\left[1 + \frac{m}{U} I\right] \text{ where } I = \int_{\theta_1}^{\theta_2} \frac{\cos\left[\frac{\alpha - \bar{\theta}}{\theta_2 - \theta_1}\pi\right] d\alpha}{\cos\theta - \cos\alpha} \qquad \ldots\ldots (11)$$

$$\text{and} \quad \frac{q_n}{U} = \begin{cases} \frac{m}{U}\pi\cos\left(\frac{|\theta| - \bar{\theta}}{\theta_2 - \theta_1}\right) & \text{for } \theta_1 \leq |\theta| \leq \theta_2 \\ 0 & \text{for all other } \theta \end{cases}$$

Let $(\theta_2 - \theta_1)$ be chosen such that $\dfrac{\pi}{\theta_2 - \theta_1}$ = an integer n.

Then

$$I \equiv I_n = \int_{\theta_1}^{\theta_2} \frac{\cos n(\alpha - \bar{\theta})}{\cos\theta - \cos\alpha}\, d\alpha = \cos n\bar{\theta} \int_{\theta_1}^{\theta_2} \frac{\cos n\alpha}{\cos\theta - \cos\alpha}\, d\alpha + \sin n\bar{\theta} \int_{\theta_1}^{\theta_2} \frac{\sin n\alpha}{\cos\theta - \cos\alpha}\, d\alpha$$

$$= \cos n\bar{\theta}\, I_{c_n} + \sin n\bar{\theta}\, I_{s_n} \qquad \ldots\ldots (12)$$

where

$$I_{c_n} = \int_{\theta_1}^{\theta_2} \frac{\cos n\alpha}{\cos\theta - \cos\alpha}\, d\alpha \text{ and } I_{s_n} = \int_{\theta_1}^{\theta_2} \frac{\sin n\alpha}{\cos\theta - \cos\alpha}\, d\alpha$$

It can be shown that I_c and I_s satisfy the following recurrence formulae:-

$$I_{c_n} + I_{c_{n-2}} = 2\cos\theta\, I_{c_{n-1}} - \frac{4}{n-1}\sin(n-1)\frac{\theta_2 - \theta_1}{2}\cos(n-1)\bar{\theta} \qquad (13)$$

$$I_{s_n} + I_{s_{n-2}} = 2\cos\theta\, I_{s_{n-1}} - \frac{4}{n-1}\sin(n-1)\frac{\theta_2 - \theta_1}{2}\sin(n-1)\bar{\theta} \qquad (14)$$

By successive reduction of these formulae, expressions can be obtained giving I_{c_n} in terms of I_{c_0} and I_{s_n} in terms of I_{s_1}; I_{c_0} and I_{s_1} can be evaluated to give

$$I_{c_0} = -\frac{1}{\sin\theta}\ln\left|\frac{\cos\bar{\theta} - \cos\left\{\theta + \dfrac{\theta_2 - \theta_1}{2}\right\}}{\cos\bar{\theta} - \cos\left\{\theta - \dfrac{\theta_2 - \theta_1}{2}\right\}}\right| \text{ and } I_{s_1} = \ln\left|\frac{\cos\theta - \cos\theta_2}{\cos\theta - \cos\theta_1}\right|$$

Finally, by using (12), the following general formula emerges for I_n:-

$$I_n = \cos n\bar{\theta}\cos n\theta\, I_{c_0} + \sin n\bar{\theta}\frac{\sin n\theta}{\sin\theta} I_{s_1} - \cos n\bar{\theta}\frac{\sin n\theta}{\sin\theta}(\theta_2 - \theta_1)$$

$$-\sum_{m=1}^{n-1}\frac{\sin m\theta}{\sin\theta}\cdot\frac{4}{n-m}\sin(n-m)\left\{\frac{\theta_2 - \theta_1}{2}\right\}\cos m\bar{\theta}\,. \qquad \ldots\ldots (15)$$

3.5 From equations (11) and (15) the velocity distribution around the cylinder corresponding to chosen values of $\bar{\theta}$ and $(\theta_2 - \theta_1)$ can be computed.

NON-DIMENSIONAL COEFFICIENTS

4.1 SUCTION QUANTITY COEFFICIENT

A suction quantity coefficient - which is a non-dimensional measure of the quantity of suction applied - can be defined as

$$S = \frac{\text{Quantity of fluid sucked through unit length of surface in unit time}}{2\,Ub} = \frac{V}{2\,Ub}$$

where U = free stream velocity and b = semi-minor axis of ellipse.

Now $$V = 2\pi m \int_0^{\pi/2} \cos\eta\,(a^2 \sin^2\eta + b^2 \cos^2\eta)^{\frac{1}{2}}\,d\eta$$

which, on integrating, becomes

$$2\pi ma \left[0.5 + \frac{1-k^2}{2k} \ln \sqrt{\frac{1+k}{1-k}}\right] \quad \text{where} \quad k^2 = 1 - \frac{b^2}{a^2}$$

$$\therefore \quad S = \pi \cdot \frac{m}{U} \cdot \frac{a}{b} \left[0.5 + \frac{1-k^2}{2k} \ln \sqrt{\frac{1+k}{1-k}}\right] \qquad \ldots\ldots (16)$$

4.2 CONDITIONS FOR INCIPIENT CAVITATION

The pressure and velocity at any point on the ellipse will be governed by the free stream conditions and the shape of the ellipse. Let the free stream pressure be denoted by P. At the point of minimum pressure on the ellipse, (where, it follows, the velocity will be maximum) let the pressure and velocity be denoted by p_c and q_c respectively. Cavitation will occur first at this point and will commence when p_c = vapour pressure of the fluid. These parameters are related by Bernoulli's theorem thus:-

$$P + \tfrac{1}{2}\rho U^2 = p_c + \tfrac{1}{2}\rho q_c^2 \qquad \ldots\ldots (17)$$

where ρ is the density of the fluid.

Furthermore, to describe the conditions under which cavitation occurs use will be made of the cavitation number Q, which is defined as

$$Q = \frac{P - p_c}{\tfrac{1}{2}\rho U^2} \qquad \ldots\ldots (18)$$

Combining (17) and (18) gives

$$Q = \left(\frac{q_c}{U}\right)^2 - 1 \qquad \ldots\ldots (19)$$

By putting p_c = vapour pressure of the fluid, free stream conditions corresponding to incipience of cavitation can be deduced from the value of Q.

5. DESCRIPTION OF COMPUTATIONS

A. FLOW PAST AN ELLIPTIC CYLINDER WITH SUCTION APPLIED OVER THE ENTIRE FORWARD HALF

5.1 Using equation (9), velocity distributions were computed corresponding to varying rates of suction for the following elliptic cylinders:-

$$\frac{b}{a} = 1, 0.866, 0.707, 0.5, 0.332, 0.2.$$

The results of these computations for a typical case $(b/a = 0.5)$ are presented graphically in Figures 1, 2 and 3. It will be observed (Figure 1) that flows with suction possess two suction peaks - one on the forward half and the other on the rear half of the cylinder. These peaks are plotted separately against S giving the two curves shown in Figure 2: their intersection gives the optimum suction peak. In Figure 3, a comparison is given of flow with optimum suction and flow in the absence of suction.

5.2 Similar curves were drawn for the other five elliptic cylinders; these results are summarised in Figure 4 where peak velocity is plotted against b/a.

5.3 From (19) and the values of q_c/U evaluated for each ellipse, the corresponding values of Q can also be calculated. Rewriting (18) in the form

$$U^2 = \frac{P - p_c}{\frac{1}{2}\rho Q}$$

enables values of U corresponding to any value of P to be calculated for conditions of incipient cavitation. The results of such calculations with water at 70°F are presented in Figure 5. The three cases dealt with indicate the extent by which the free stream velocity can be increased with optimum suction. This point is further illustrated in Figure 6 where U is plotted against b/a for a free stream pressure of 15 lbs/sq.in. With $b/a > 0.3$, optimum suction considerably delays the onset of cavitation: for example, with $b/a = 0.5$, the free stream speed can be more than doubled before the inception of cavitation.

B. FLOW PAST A CIRCULAR CYLINDER WITH SUCTION OVER LIMITED AREAS

5.4 In this case, the computing programme undertaken was designed to determine the effect on the suction peak of suction area location and extent at various rates of suction. Calculations were made for the following values of $(\theta_2 - \theta_1)$ and $\bar{\theta}$:-

$(\theta_2 - \theta_1)$	90	60	30	20	15	12
$\bar{\theta}$	45	30, 45, 60	15, 30, 45, 60, 75	15, 30, 45, 60, 75	15, 30, 45, 60, 75	15, 30, 45, 60, 75

5.5 The results of these calculations are presented in Figures 7 and 8. In Figure 7, peak velocity is plotted against $\bar{\theta}$ for each value of $(\theta_2 - \theta_1)$ and curves are drawn relating these parameters at constant values of S: furthermore, for each value of $(\theta_2 - \theta_1)$ a curve relating optimum peak velocity and $\bar{\theta}$ is also given.

5.6 Figure 7 shows that, for any $(\theta_2 - \theta_1)$, a curve of peak velocity against $\bar{\theta}$ for constant S either

(1) falls with increasing $\bar{\theta}$ to a minimum where it meets the optimum curve, or

(2) remains above the optimum curve over the entire range of $\bar{\theta}$.

In the latter case it will be seen that the lowest value of the peak velocity occurs at the upper limit of $\bar{\theta}$, at which point $\theta_2 = 90°$. Study of cases obeying (1), indicates that, with increasing $(\theta_2 - \theta_1)$ and for any particular value of S, the minimum peak velocity decreases while the corresponding value of $\bar{\theta}$ increases. In the limit, the value of $(\theta_2 - \theta_1)$ will be such that the S curve and the optimum curve meet at the upper limit of $\bar{\theta}$; that is, where $\theta_2 = 90°$. Hence, for any S, the optimum values of $(\theta_2 - \theta_1)$ and $\bar{\theta}$ always satisfy the condition $\theta_2 = 90°$. In order to determine the optimum combination of $(\theta_2 - \theta_1)$ and $\bar{\theta}$ for any S, values of the peak velocity on the forward and rear half of the cylinder are plotted against values of $\bar{\theta}$ for which $\theta_2 = 90°$ in Figure 8. A pair of curves can then be drawn for any value of S one giving the peak velocity on the forward half and the other the peak velocity on the rear half. The point of intersection of any such pair gives the optimum values of $\bar{\theta}$ and the peak velocity, whereas the corresponding value of $(\theta_2 - \theta_1)$ is given by $(\theta_2 - \theta_1) = 2\,(90 - \bar{\theta})$.

NUMERICAL RESULTS

5.7 While it has been shown that distributed suction can considerably delay the onset of cavitation, the practicability of the method must obviously depend on the rate of suction required. The following tables give the permissible free stream speeds at conditions of incipient cavitation corresponding to various suction rates expressed in gallons per minute.

A - FLOW PAST ELLIPTIC CYLINDERS WITH A DISTRIBUTION OF SINKS OVER THE ENTIRE FORWARD HALF OF STRENGTH PROPORTIONAL TO $\cos\eta$

TABLE 1: $\frac{b}{a} = 1$ and $P = 15$ lbs/sq. in.

S	$\frac{q_c}{U}$	Q	U	Suction rate per foot length of cylinder of diameter 2" - gallons per minute
0.0	2	3	26.9	0
0.05	1.960	2.842	27.6	86
0.10	1.923	2.698	28.4	178
0.20	1.849	2.419	30.0	375
0.50	1.630	1.657	36.2	1130
1.00	1.320	0.742	54.1	3380
1.21(opt)	1.209	0.462	68.5	5180

TABLE 2: $\frac{b}{a} = 0.5$ and $P = 15$ lbs/sq. in.

S	$\frac{q_c}{U}$	Q	U	Suction rate per foot length of cylinder with $b = 1$" - gallons per minute
0.0	1.5	1.25	41.7	0
0.05	1.478	1.184	42.8	134
0.10	1.455	1.117	44.1	276
0.20	1.418	1.011	46.3	579
0.50	1.318	0.737	54.3	1700
1.00	1.180	0.392	74.4	4650
1.19(opt)	1.130	0.277	88.5	6580

TABLE 3: $\frac{b}{a} = 0.2$ and P = 15 lbs/sq. in.

S	$\frac{q_c}{U}$	Q	U	Suction rate per foot length of cylinder with b = 1" - gallons per minute
0.0	1.20	0.44	70.3	0
0.05	1.190	0.416	72.2	226
0.10	1.180	0.392	74.4	465
0.20	1.166	0.360	77.7	970
0.30(opt)	1.160	0.340	79.2	1485

B - FLOW PAST A CIRCULAR CYLINDER WITH A DISTRIBUTION OF SINKS OVER LIMITED AREAS OF STRENGTH PROPORTIONAL TO $\cos\left[\left(\frac{|\alpha| - \bar{\theta}}{\theta_2 - \theta_1}\right)\pi\right]$

TABLE 4: P = 15 lbs/sq. in.

S	Optimum Values			Q	U	Suction rate per foot length of cylinder of diameter 2" - gallons per minute
	$\bar{\theta}$	$(\theta_2 - \theta_1)$	$\frac{q_c}{U}$			
0.0	-	-	2	3	26.9	0
0.03	70°	40°	1.945	2.783	27.9	52
0.06	65½°	49°	1.905	2.629	28.7	108
0.10	63½°	53°	1.860	2.460	29.7	186
0.15	62°	56°	1.810	2.276	30.9	290
0.20	60°	60°	1.770	2.133	31.9	399
0.25	58°	64°	1.725	1.976	33.2	519

5.8 It is clear from the tables of 5.7, that in order to effect an appreciable delay in the onset of cavitation, an excessive rate of suction is required. For this reason alone, it is unlikely that the method of distributed suction can be usefully employed in practice, at least on non-lifting two-dimensional forms.

6. SUMMARY AND CONCLUSIONS

Consideration is given to the possibility of using distributed suction to reduce the suction peak in the pressure distribution on a body in two-dimensional flow and so delay the onset of cavitation. Flow equations are derived for two cases:

(a) flow past elliptic cylinders with suction applied over the entire forward half, and

(b) flow past circular cylinders with suction applied over limited areas.

Calculations have been made to determine the effect of varying amounts of suction and, in the case of (b), the added effect of changing the location and extent of the suction area. These results are presented graphically. While it has been shown that the onset of cavitation can be considerably delayed (for example, a circular cylinder with optimum suction cavitates for the same free stream conditions as an elliptic cylinder of fineness ratio 5:1 in the absence of suction) the rate of suction required to effect such an improvement is excessive: even a small improvement requires a considerable rate of suction. For this reason, it is unlikely that the method can be usefully employed in practice, at least on non-lifting two-dimensional forms.

ACKNOWLEDGEMENTS

Acknowledgement is due to the Admiralty for permission to publish this paper.

This investigation was undertaken at the suggestion of Mr. I. J. Campbell; his helpful advice and guidance during the course of its preparation are gratefully acknowledged.

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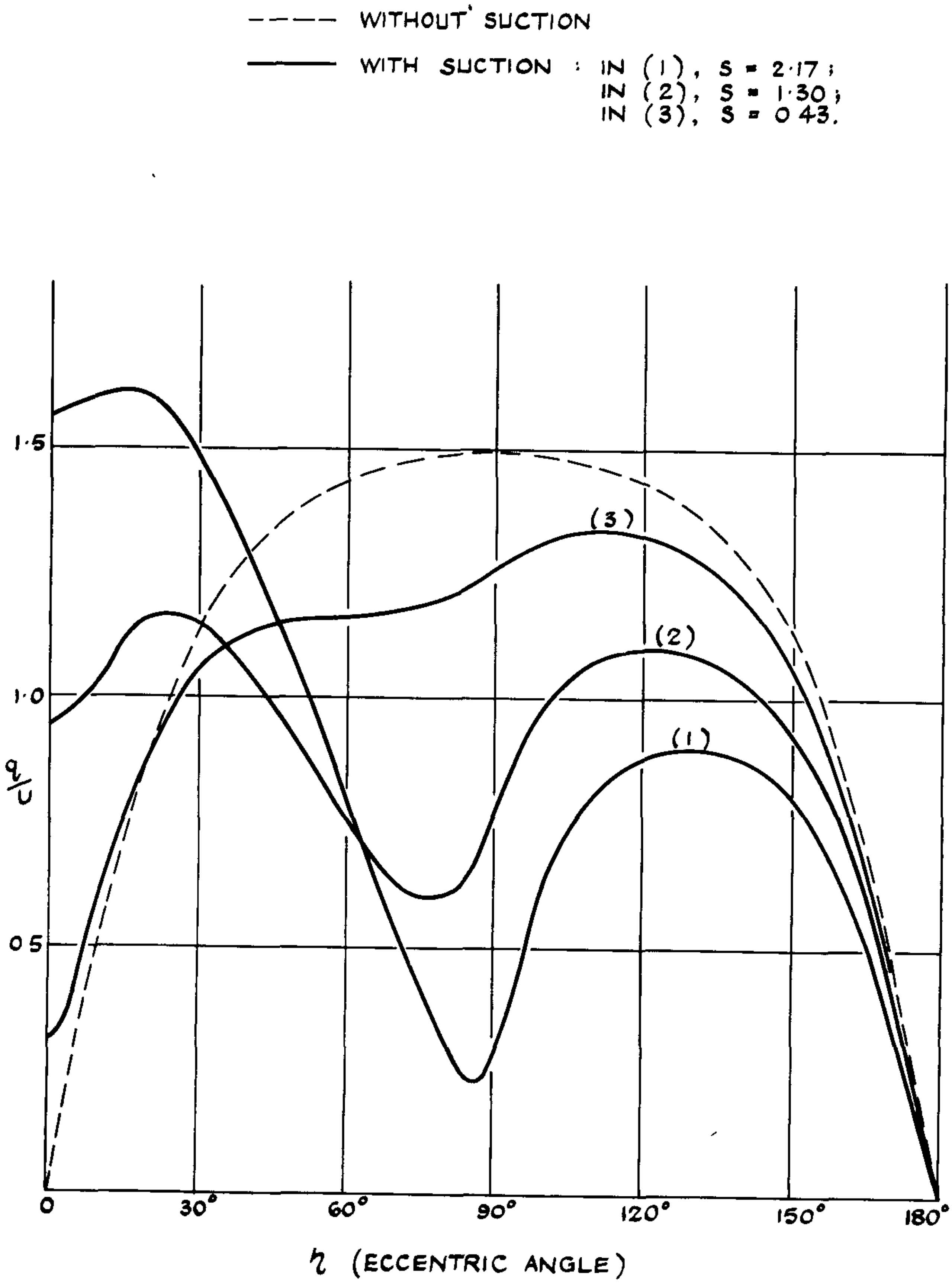
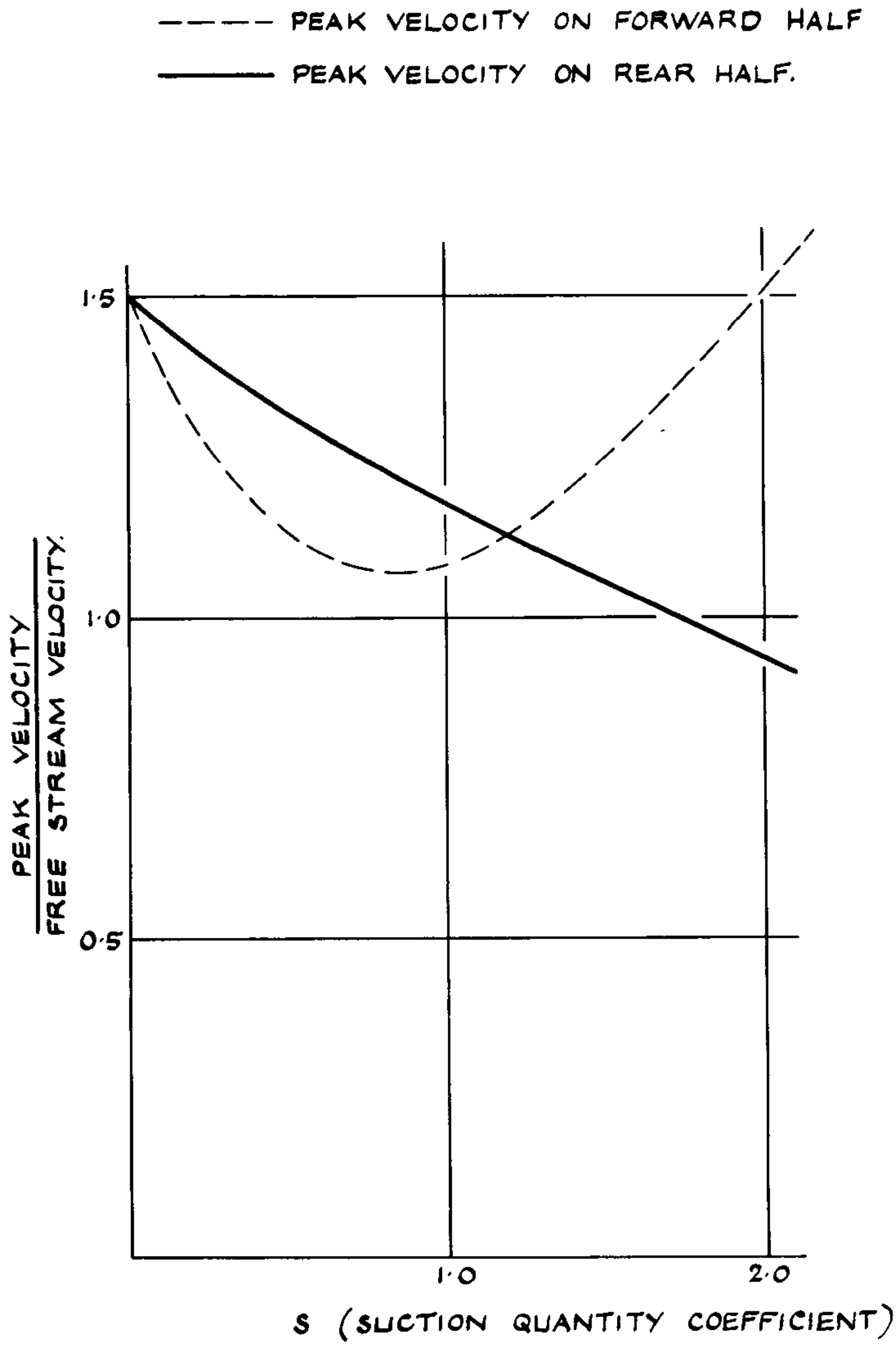


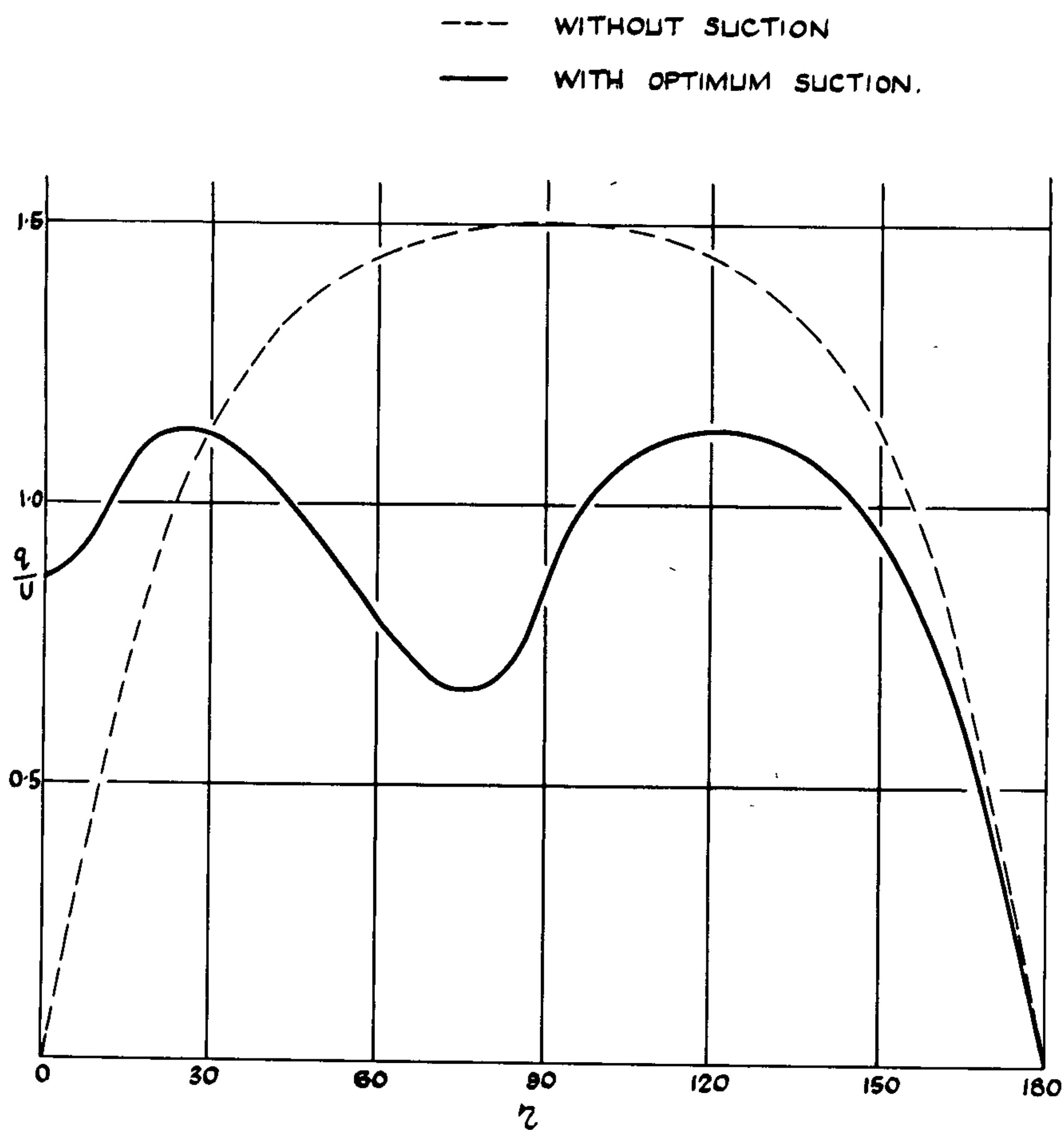
TWO-DIMENSIONAL FLOW PAST AN ELLIPTIC CYLINDER ($b/a = 0{\cdot}5$) AT ZERO INCIDENCE

FIG. 1.



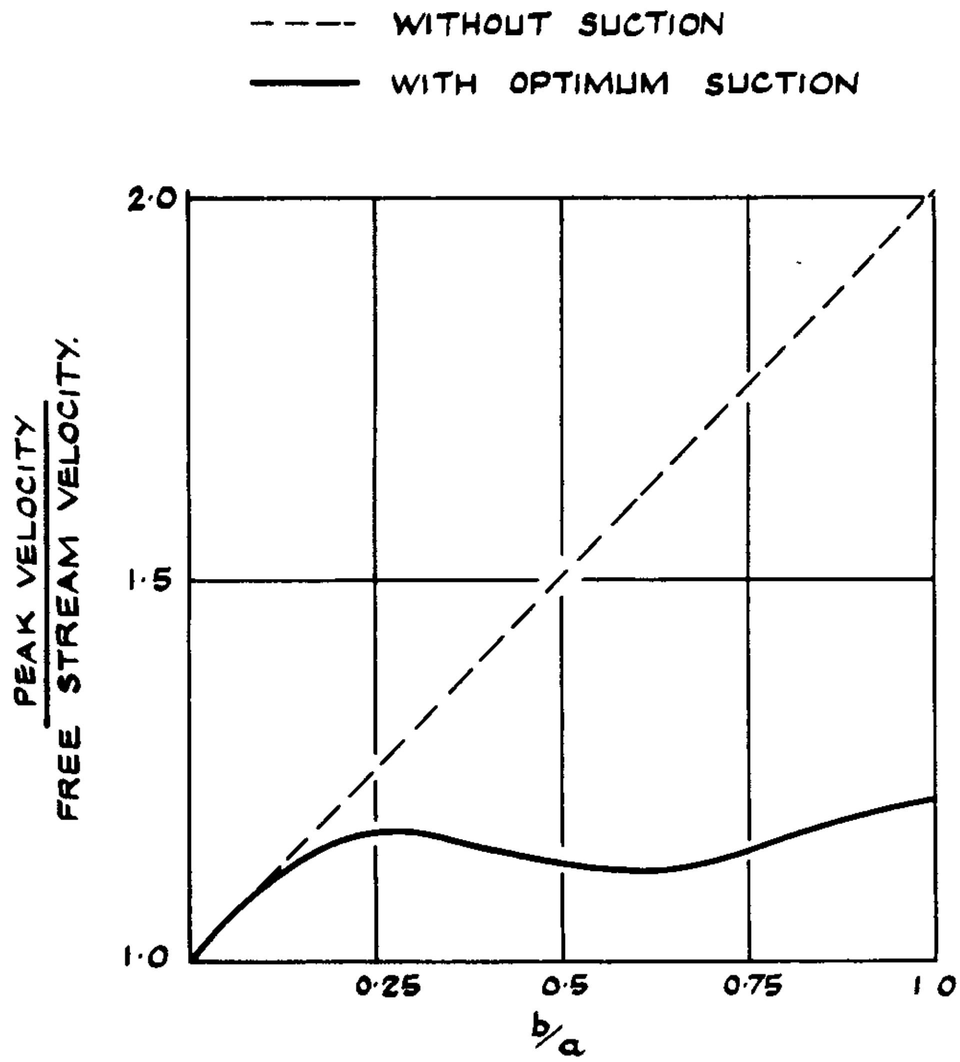
TWO-DIMENSIONAL FLOW PAST AN ELLIPTIC CYLINDER ($b/a = 0 \cdot 5$) AT ZERO INCIDENCE

FIG. 2.



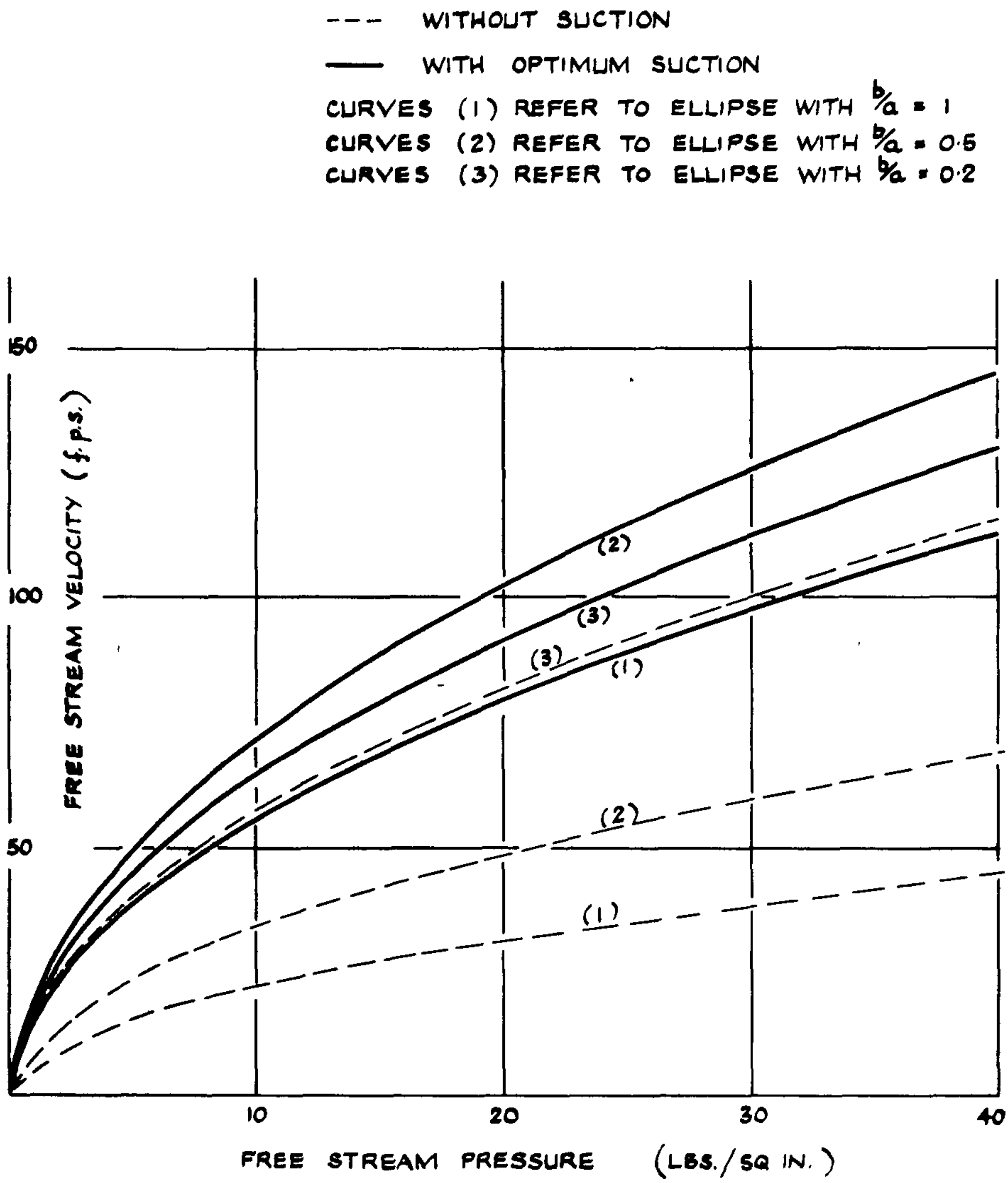
TWO-DIMENSIONAL FLOW PAST AN ELLIPTIC CYLINDER ($b/a = 0.5$) AT ZERO INCIDENCE

FIG.3.



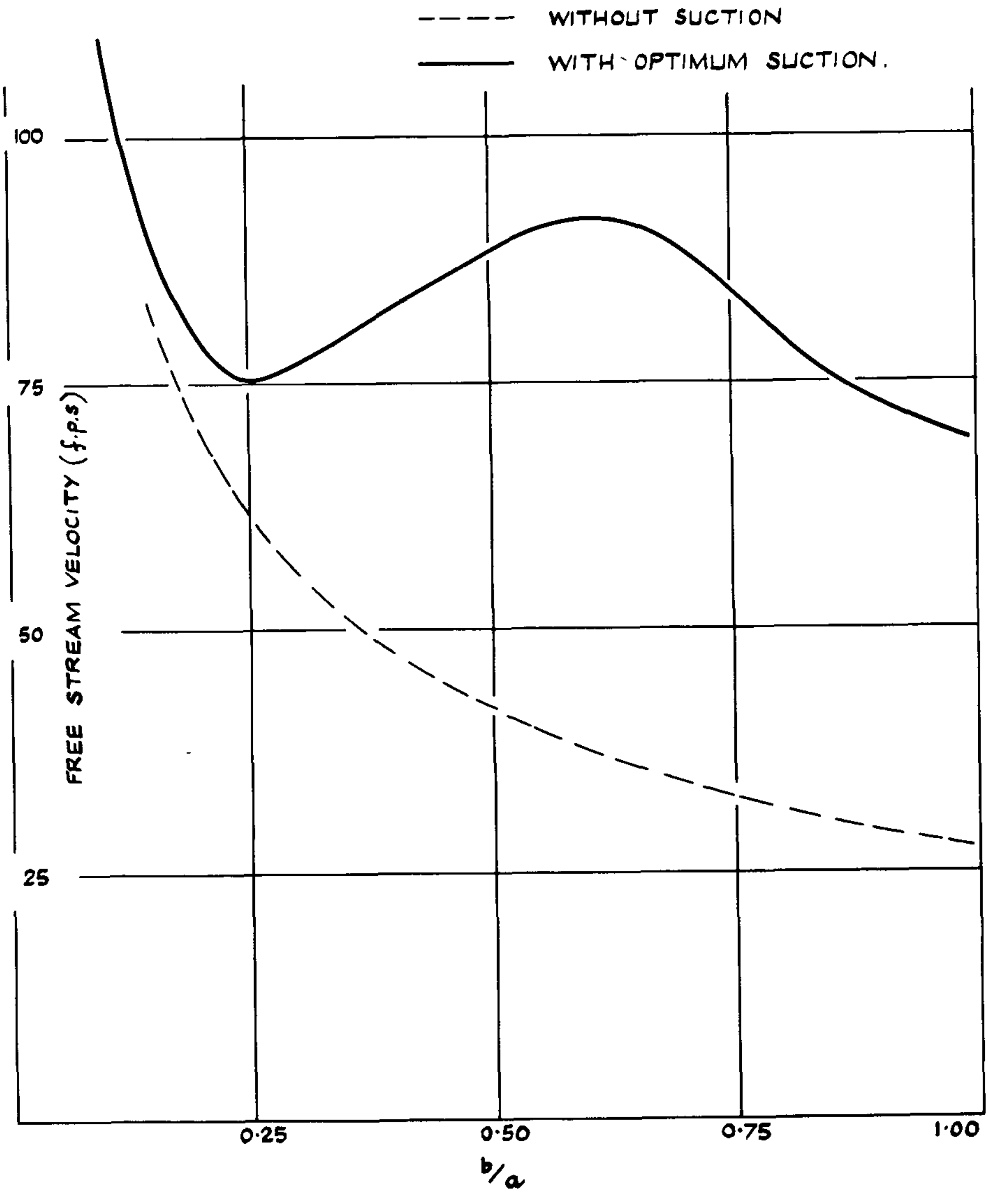
TWO-DIMENSIONAL FLOW PAST ELLIPTIC CYLINDERS AT ZERO INCIDENCE.

FIG. 4.



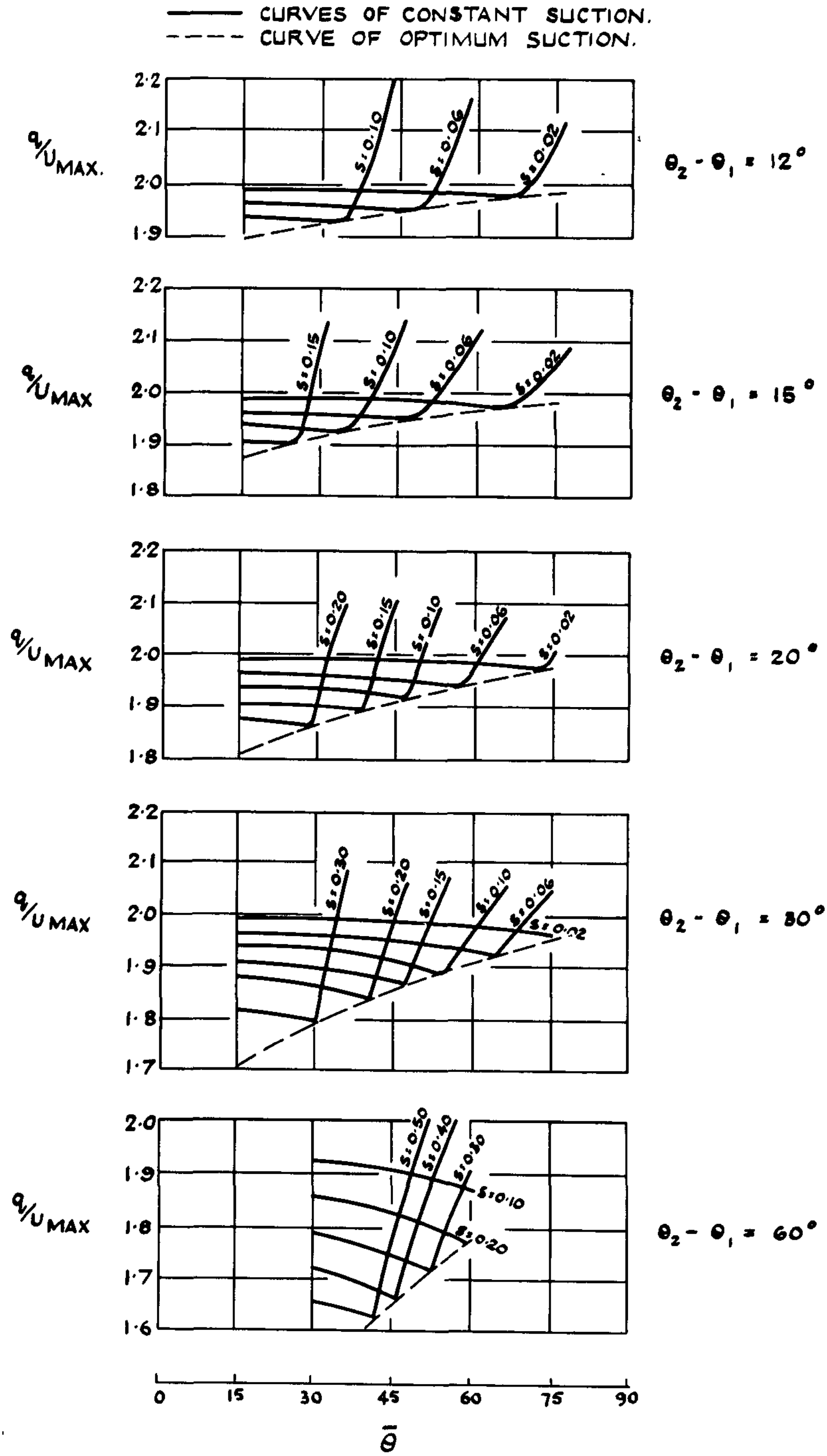
FREE STREAM CONDITIONS CORRESPONDING TO INCIPIENCE OF CAVITATION FOR TWO-DIMENSIONAL FLOW PAST ELLIPTIC CYLINDERS AT ZERO INCIDENCE.

FIG. 5.



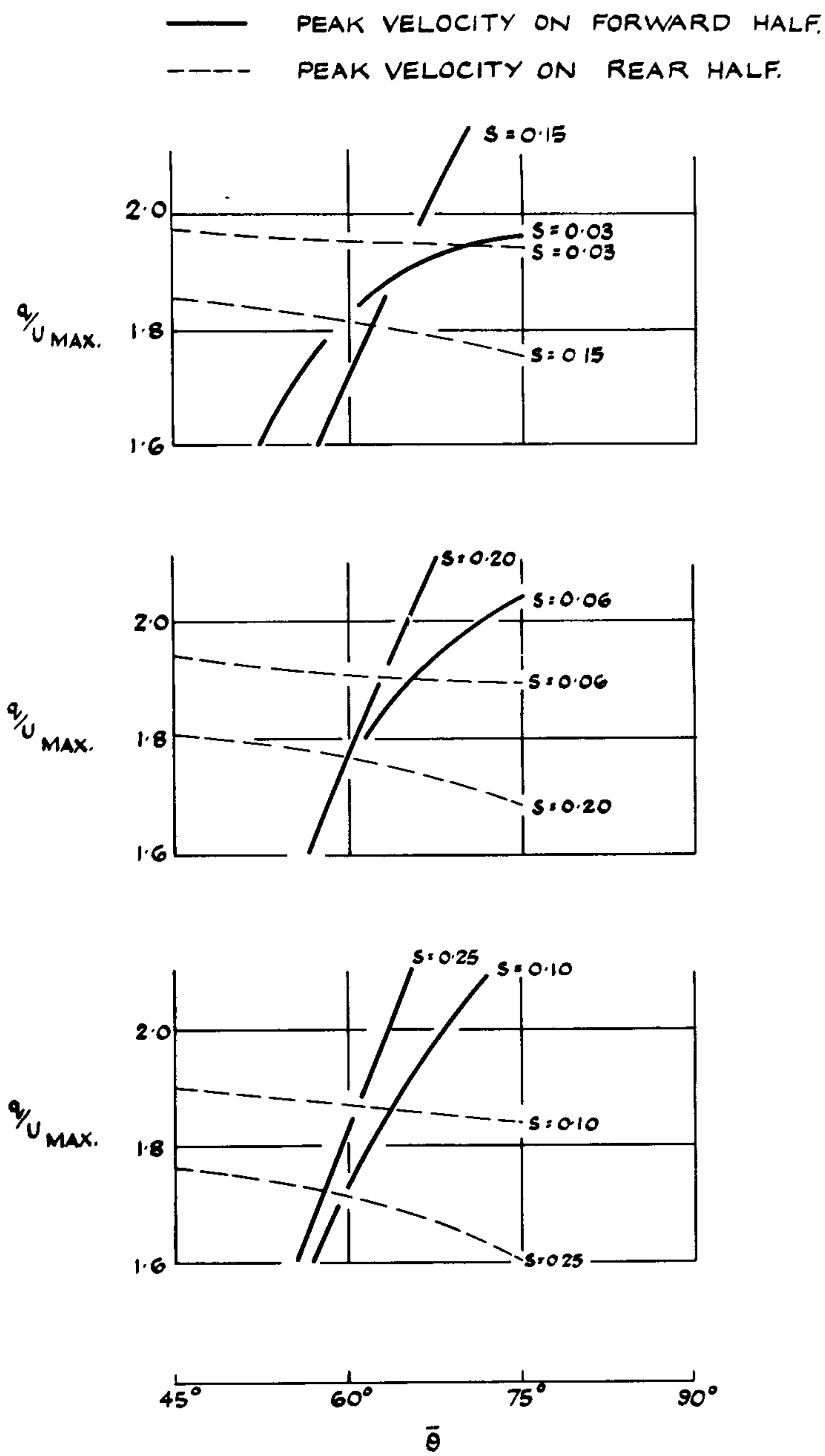
INCIPIENT CAVITATION SPEEDS AT FREE STREAM PRESSURE OF 15 LBS./SQ.IN. FOR TWO-DIMENSIONAL FLOW PAST ELLIPTIC CYLINDERS AT ZERO INCIDENCE.

FIG.6.



TWO-DIMENSIONAL FLOW PAST A CIRCULAR CYLINDER WITH SUCTION APPLIED OVER LIMITED AREAS

FIG.7.



DETERMINATION OF OPTIMUM LOCATION OF SUCTION AREA CORRESPONDING TO DIFFERENT VALUES OF S FOR TWO-DIMENSIONAL FLOW PAST A CIRCULAR CYLINDER.

FIG. 8.

C.P. No. 362

(18,531)
A.R.C Technical Report

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S O Code No 23-9010-62

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